Evaluation of Fluid-Thermal Systems by Dynamic Data Driven Application Systems -Part II

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Abstract. A Dynamic Data Driven Application Systems (DDDAS) methodology is developed for evaluation of fluid-thermal systems wherein a complete specification of the boundary conditions is not known *a priori* and experimental diagnostics are restricted to a limited region of the flowfield. The Closed Loop formulation of DDDAS is used whereby experiment and simulation are synergized in an iterative manner to determine the unknown boundary conditions, thereby enabling a full simulation (and hence, evaluation) of the fluid-thermal system. In this DDDAS methodology, the experiment directs the simulation and vice-versa. The DDDAS methodology is applied to a heated jet injected into a laminar boundary layer where the jet temperature and velocity are not known *a priori* for the simulations. The DDDAS methodology accurately determines the unknown jet temperature and velocity.

1 Introduction

In a wide range of fluid-thermal systems, there is typically limited access to the flow domain for experimental measurements of the flowfield (*e.g.*, pressure, species concentration, temperature and velocity). Examples of such systems include combustors, furnaces and reactors. For example, an optical fiber drawing furnace typically has an infrared sensor to monitor the temperature of the heating element at a single location [1]. Consequently, the necessary boundary conditions (*e.g.*, inflow, outflow, solid boundary, etc) for computational simulations (using a Computational Fluid Dynamics [CFD] code such as Fluent[©]) are not completely known, and therefore a simulation cannot be performed.

The objective of this research is the development of a Dynamic Data Driven Applications Systems methodology that synergizes experiment and simulation in fluid-thermal systems to determine the unknown boundary conditions, thereby enabling a complete simulation of the fluid-thermal system.

2 Dynamic Data Driven Application Systems

The Dynamic Data Driven Applications Systems (DDDAS) concept was described in the DDDAS Workshop held at the National Science Foundation in March 2000 [2] and further described by Darema [3] (see also the DDDAS webpage [4]). DDDAS is a unique approach to engineering and scientific research wherein experiment and simulation interact in a synergistic, symbiotic manner. There are two different implementations of DDDAS: Open Loop and Closed Loop. In Open Loop, experimental data is streamed into the simulation (or vice-versa) to achieve greater accuracy, detail and/or robustness. An example is the Dynamic Data Driven Wildfire Modeling methodology of Mandel *et al* [5] and Douglas *et al* [6]. In Closed Loop, experiment and simulation interact in an iterative manner, *i.e.*, the experiment guides the simulation and the simulation in turn guides the experiment [3]. An example is the Dynamic Data Driven Optimization Methodology (DDDOM) developed by Knight *et al* [7,8].

3 Description of Research

3.1 Objective

The objective is the development of a DDDAS methodology for synergizing experiment and simulation to evaluate fluid-thermal systems wherein the experimental measurements are restricted in region and scope, and the *a priori* boundary conditions for simulation are incomplete. The Closed Loop DDDAS concept is used wherein the experiment directs the simulation and vice-versa in an iterative manner. The strategy is to approximate the unknown boundary conditions by minimizing the error in the prediction of the measured data (*i.e.*, the experiment driving the simulation), and to identify needed subsequent experimental measurements to reduce the error (*i.e.*, the simulation driving the simulational simulations to reduce the error (*i.e.*, the experiment driving the simulation).

3.2 Configuration

We consider a rectangular jet injected perpendicular to an incompressible laminar boundary layer. The configuration is shown in Fig. 1. The inflow is an equilibrium laminar boundary layer in air defined by the specified freestream conditions (velocity U_{∞} , static pressure p_{∞} and static temperature T_{∞}) and boundary layer thickness δ_{∞} (*i.e.*, the laminar boundary layer thickness that would exist at the location of the jet exit in the absence of the jet). The jet is defined by the jet average velocity U_j , static pressure p_j , and static temperature T_i . The computational domain ABCDE is shown. For the simulations, the freestream conditions (velocity U_{∞} , static pressure p_{∞} , static temperature T_{∞} and boundary layer thickness δ_{∞}) are assumed known. By analogy to the optical fiber furnace, the jet average velocity U_i and static temperature T_i are assumed unknown (insofar as the simulations are concerned), while the jet exit pressure p_i is assumed known. The objective is the determination of the jet average velocity U_j and static temperature T_j based upon a Closed Loop DDDAS methodology. The range of values for U_i and T_j provided to the DDDAS methology are indicated in Table 1 (see Section 3.7).



Fig. 1. Flow configuration

3.3 Experiments

The experiments were performed in the Rutgers Low Speed Wind Tunnel. The experimental configuration is shown in Fig. 2a. A two-dimensional slot jet protrudes from a flat plate with the jet centerline at a distance of 188 mm from the leading edge of the plate. The flat plate has a sharp leading edge and is raised 50 mm above the wind tunnel floor to avoid the tunnel floor boundary layer. The jet slot width is 3.2 mm and the spanwise depth is 545 mm. The jet fences protrude 8.8 mm above the flat plate and each fence is 6.4 mm wide in the x-direction. The jet exit temperature was measured by a small bead thermocouple at the jet exit and was observed to vary less than 2% across the jet exit. Additional details are presented in Knight *et al* [9].

A diode laser system was used to measure the time-varying absorbance across the flowfield in the spanwise direction at selected locations. The measured laser absorbance is related to the local thermodynamic conditions and gas concentrations through the spectral absorption coefficient and Beer's law

$$A = 1 - \frac{I}{I_o} = 1 - \exp\left(-k_v L\right)$$

where $k_v = S\phi P$, S is the temperature dependent linestrength (cm²-cm⁻¹), ϕ is the lineshape function (1/cm⁻¹), P is the partial pressure of the absorbing species given in terms of number density (cm⁻³), and L is the path length (cm). The spectrally-dependent absorbance was converted from the time domain to the wavelength domain using laser calibration tuning curves. The current injection versus wavelength tuning was determined using an optical spectrum analyzer prior to performing the experiments. The spectrally-dependent absorbance (k_n) can be integrated versus wavelength to remove the effect of the lineshape



(a) Wind tunnel model



(b) Diode laser configuration

Fig. 2. Experiment

function. The integrated absorbance (k) only depends on the linestrength and number density of absorbers. The temperature dependency of both quantities is known, and therefore the path-averaged temperature can be obtained from the absorption data. Further details are presented in Ma *et al* [10].

3.4 Simulations

The two-dimensional, laminar, unsteady Navier-Stokes equations were solved using Fluent[©]. The fluid is air. The Incompressible Ideal Gas Law was used together with the Boussinesq approximation. The molecular dynamic viscosity was modeled using Sutherland's Law. The simulations are second-order accurate in space and time. The spatial reconstruction is 3rd order MUSCL, and the temporal integration is Implicit Dual-Time Stepping. Twenty inner time steps at a specified inner Courant number of five are used per outer (physical) time step. A constant outer timestep $\Delta t = 4 \cdot 10^{-4}$ sec was used for all simulations corresponding to an outer Courant number $CFL = \Delta t U_{\infty} / \Delta x_{min} = 4$ to 8 for the range 4 m/s $\leq U_{\infty} \leq 8$ m/s considered in this study. Further details are presented in Knight *et al* [9]. Table 1 summarizes the range of parameters for the simulations.

3.5 Validation

A validation study was performed to assess the accuracy of the simulations by comparison with experiment. Details are presented in Knight *et al* [9]. An experiment was performed with $U_{\infty} = 4$ m/s, $T_{\infty} = 299$ K, $p_{\infty} = 101$ kPa, $U_j = 8.11$ m/s, $T_j = 398$ K and $p_j = 101$ kPa. The mean temperature was measured at three locations in the flowfield downstream of the jet using the diode laser absorbance method (Section 3.3) and thermocouple. The freestream and jet pressure, temperature and velocity conditions were provided to the simulation using Fluent[©]. The computed mean temperature at the three locations within the flowfield agreed with the experimental mean temperature within 10 K. This represents also the uncertainty in the experimental measurement.

3.6 Response Surface Models

The energy equation is decoupled from the mass and momentum equations (neglecting variations in density and buoyancy effects), and thus the static temperature behaves as a passive scalar. The temperature field must therefore scale as $T(x, y, t) - T_{\infty} = (T_j - T_{\infty})f(x, y, t; U_j, U_{\infty})$. Therefore, a quadratic Response Surface Model (RSM) for the time mean static temperature $T_m(x, y)$ may be constructed at a fixed position (x, y) in the flowfield according to

$$T_m(x,y) - T_{\infty} = (T_j - T_{\infty}) \left[\beta_o(x,y) + \beta_1(x,y) \left(\frac{U_j}{U_{\infty}}\right) + \beta_2(x,y) \left(\frac{U_j}{U_{\infty}}\right)^2 \right]$$

The coefficients $\beta_i(x, y)$ are obtained from simulations performed for a fixed value $T_j - T_{\infty}$ (selected from the range indicated in Table 1) and a set of U_j selected from the range indicated in Table 1 For this study, the values $U_j = 4$, 6 and 8 m/s were selected. The freestream conditions $(U_{\infty}, T_{\infty}, p_{\infty})$ and jet pressure p_j are fixed as indicated in Table 1.

3.7 DDDAS Methodology

The Closed Loop DDDAS methodology integrates experiment and simulation in a synergistic, iterative manner to achieve a complete evaluation of the fluidthermal system. There are five steps:

- 1. Select Monitor Locations for Simulations A set S_s of monitor locations for the simulations is selected. At each monitor location, a time series of the static temperature is obtained in every simulation. The number of monitor locations can be arbitrarily large and is limited only by available disk storage for the time series data. A total of eighteen monitor locations were selected (Table 2).
- 2. Generate Response Surface Model Based on Simulations for Fixed ΔT_j^i A fixed value of $\Delta T_j^i = T_j^i - T_\infty$ (i = 1, 2, ...) is chosen from within the range of values indicated in Table 1. Simulations are performed for a set of values U_j for the fixed ΔT_j^i and time series at each of the monitor locations in S_s is recorded. A Response Surface Model for the mean static temperature T_m at each monitor location is generated based upon the assumed value of ΔT_j^i and selected values of U_j (see Section 3.6).
- 3. Select Monitor Locations for Experiments A subset S_e^k of the monitor locations S_s is selected for the k^{th} experiment (k = 1, 2, ...). Each experiment is performed at the same U_j and T_j ; however, the values of U_j and T_j are not known for any of the simulations. Note that the size of the set S_e^k is small compared to S_s due to the substantial amount of time required for the experimental measurements.

 Table 1. Flow Conditions

- 4. Estimate Experimental Values for $T_j T_{\infty}$ and U_j The experimental mean temperatures are compared with the Response Surface Models to estimate the value of $T_j - T_{\infty}$ and U_j in the experiment (see below).
- 5. Determine New Measurement Locations

The Response Surface Model is used to select the next set of monitor locations S_e^{k+1} from S_s . Step No. 4 is repeated to provide a revised estimate of $T_j - T_{\infty}$ and U_j . Based upon the estimated value of $T_j - T_{\infty}$, the procedure repeats from Step 2 until convergence of the predicted values for U_j and T_j .

 Table 2. Location of Monitors

Parameter	· Value		No.	x (cm)	y (cm)	No.	x (cm)	y (cm)	No.	x (cm)	y (cm)
$U_{\infty} (\mathrm{m/s})$	4.0	-	1	1.2	2.0	7	1.2	3.0	13	1.2	4.0
T_{∞} (K)	290.		2	3.2	2.0	8	3.2	3.0	14	3.2	4.0
p_{∞} (kPa)	101.8		3	5.2	2.0	9	5.2	3.0	15	5.2	4.0
$U_j (m/s)$	4.0 to 8.0		4	7.2	2.0	10	7.2	3.0	16	7.2	4.0
T_j (K)	350 to 450		5	9.2	2.0	11	9.2	3.0	17	9.2	4.0
p_j (kPa)	101.8		6	11.2	2.0	12	11.2	3.0	18	11.2	4.0

The estimate of the experimental values $T_j - T_{\infty}$ and U_j at each step in the procedure is obtained as follows. The square error between the experimental mean temperature and the Response Surface Model for each possible subset of l locations within S_e^k is computed as

$$E = \sum_{l} \left\{ \Delta T_{m_e} - \Delta T_j \left[\beta_o(x, y) + \beta_1(x, y) \left(\frac{U_j}{U_\infty} \right) + \beta_2(x, y) \left(\frac{U_j}{U_\infty} \right)^2 \right] \right\}^2$$

where $\Delta T_j = T_j - T_{\infty}$, $\Delta T_{m_e} = T_{m_e} - T_{\infty}$, and the sum is over l locations within S_e^k (the minimum number for l is 2). For example, assume S_e^k contains six locations and let l = 2. For each possible set of two locations from S_e^k , the values of ΔT_j and U_j that minimize E are determined. This yields fifteen triplets $(\Delta T_j, U_j, E)$. For a given value of l, the predicted values of ΔT_j and U_j , denoted by ΔT_j^l and U_j^l , are taken to be the triplet with the minimum E (*i.e.*, the values of ΔT_j and U_j with the smallest square error). The procedure is repeated for all values of l from l = 2 to $n = \text{size } S_e^k$. The estimate for the experimental value of $T_j - T_{\infty}$ is the average of these values $T_j - T_{\infty} = (n-1)^{-1} \sum_{l=2}^{l=n} \Delta T_j^l$ and similarly for U_j .

3.8 Results

The Closed Loop DDDAS methodology was applied to determine the experimental $T_j - T_{\infty}$ and U_j . A total of eighteen monitor locations were selected (Step 1). Response Surface Models were generated for all monitor locations for an assumed value $\Delta T_j = 66$ K (Step 2). Based upon these models, six locations (Nos.

3, 9, 10, 14, 15 and 16) from Table 2 were selected for the experiment (Step 3). Note that the experimental U_j and $T_j - T_\infty$ were selected by the experimentalists (Q. Ma and T. Rossman) but not communicated to the person performing the Closed Loop DDDAS Method (D. Knight) until the DDDAS method was converged. Using the experimental mean temperature measurements at the six locations, the estimated values $\Delta T_j = 110 \pm 16$ K and $U_j = 7.3 \pm 1$ m/s were obtained using the Response Surface Models (Step 4). An additional set of locations for experiments was defined based upon the Response Surface Models (Nos. 2, 4, 5 and 17) (Step 5). A revised estimate $\Delta T_i = 120 \pm 16$ K and $U_j = 7.1 \pm 1$ m/s were obtained using the Response Surface Models (Step 4). A revised $T_j - T_{\infty} = 115$ K was selected for creation of the Response Surface Models (Step No. 2) recognizing that the value originally used $(T_i - T_{\infty} = 66 \text{ K})$ was significantly below the value predicted by the Response Surface Models. Steps 4 and 5 were repeated using the new Response Surface Models yielding the estimate $T_j - T_{\infty} = 105 \pm 13$ K and $U_j = 7.1 \pm 1$ m/s. The actual experimental values are $T_j - T_{\infty} = 107 \pm 10$ K and $U_j = 8.0$ m/s. The predicted values for $T_i - T_{\infty}$ and U_i thus agree with the experimental measurements to within the experimental uncertainty (Section 3.5), thereby validating the Closed Loop DDDAS methology.

Table 3. Results of DDDAS Method

	Predicted					
Iteration	$T_j - T_\infty$ (K)	$U_j (m/s)$				
1	110 ± 16	7.3 ± 1				
2	120 ± 16	7.1 ± 1				
3	105 ± 13	7.1 ± 1				
Exp	107 ± 10	8				

4 Conclusions

A methodology for evaluation of fluid-thermal systems is developed based upon the Dynamic Data Driven Application Systems approach. The methodology is intended for fluid-thermal systems where complete specification of the boundary conditions is not known *a priori* and experimental measurements are restricted to a subregion of the fluid-thermal domain. The methodology synergizes experiment and simulation in a closed-loop, iterative manner to achieve a full evaluation of the fluid-thermal system. Results are presented for the configuration of a heated jet injected into a laminar boundary layer where the jet temperature is not known *a priori*. The DDDAS methodology accurately predicts the unknown jet temperature and jet velocity.

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